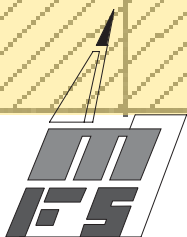


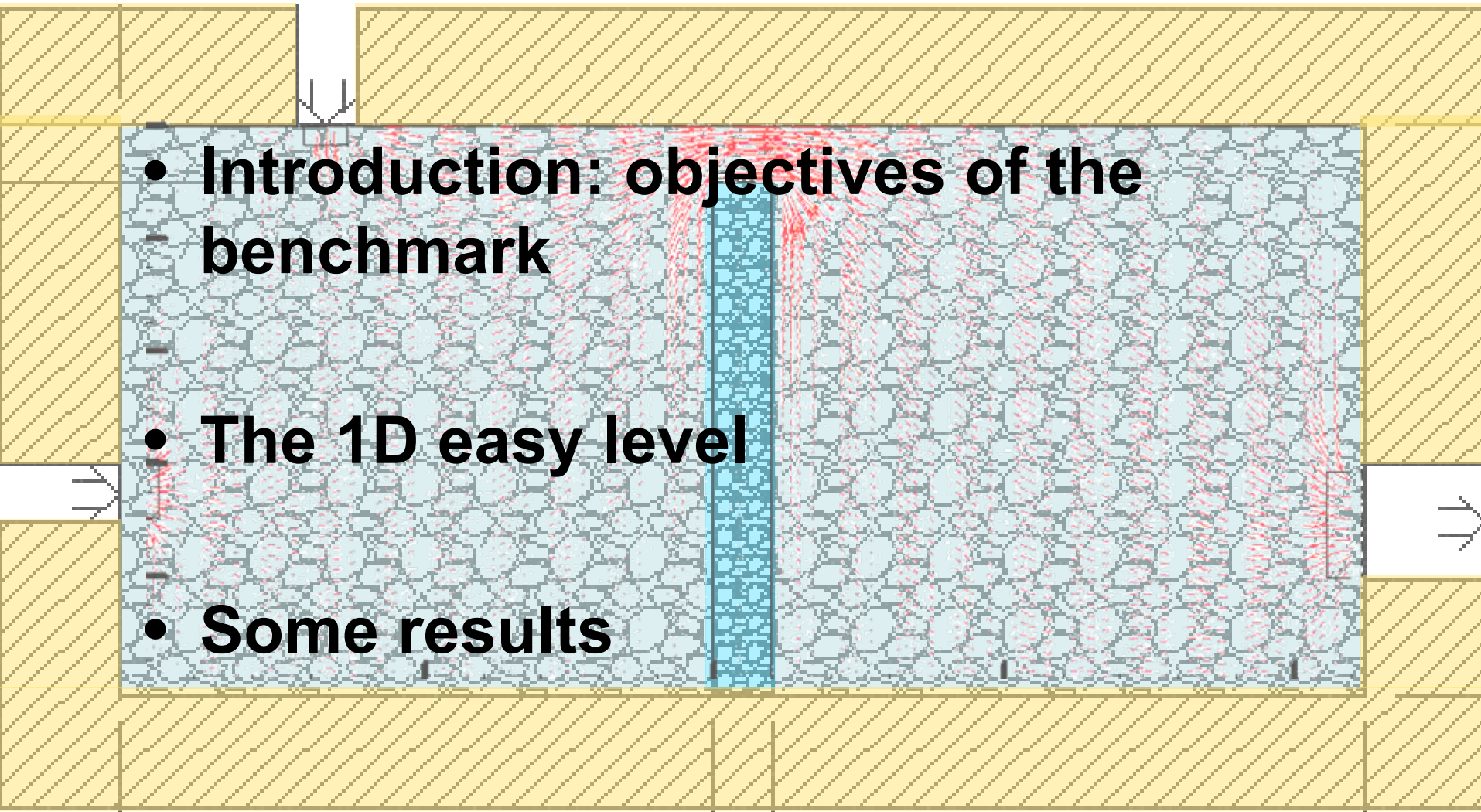
The reactive transport benchmark : A reference solution for 1D easy level ?

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Outline

- 
- **Introduction: objectives of the benchmark**
 - **The 1D easy level**
 - **Some results**



Some questions...

(about the resolution)

Operator Splitting / Global Approach

Operator Splitting:

Iterative – Non iterative

- OS scheme
- OS errors

Global Approach:

Scheme : DSA / DAE

Resolution of non linear system

CPU time / Memory

Space discretisation

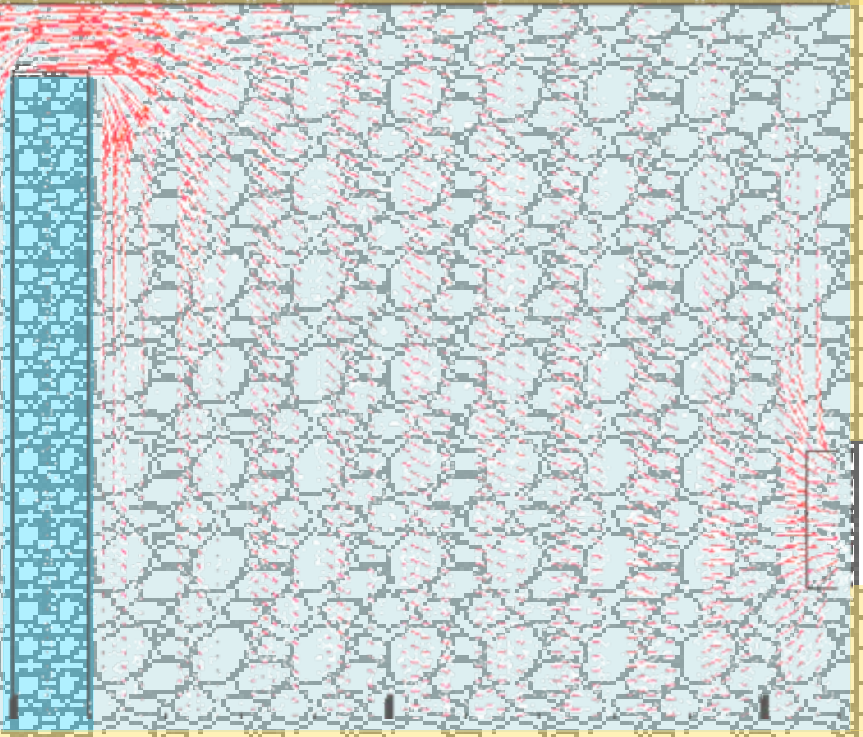
- **Objectives**

- Stability
- Numerical diffusion
- Efficiency

- Finite Elements / Volumes
- Particle Tracking
- ELLAM methods...

Time discretisation

- Explicit / Implicit
- Higher order
- Adaptive time step
 - Heuristic
 - Predictor-corrector



About convergence...

- Iterative method for chemistry
- Iterative method for transport (SIA)
- Iterative method for global approach
- What about very small concentration
 - From transport $C = 10^{-300}$...
 - Numerical problem if $C = 0$

The 1D easy-level benchmark



Medium-level

Hard-level

2D

Reactive transport modelling

$$\omega \frac{\partial (T_{M_j} + T_{F_j})}{\partial t} = -\nabla \cdot (\omega u T_{M_j}) + \nabla \cdot (D \cdot \nabla T_{M_j})$$

Advection – Diffusion – Reaction equation

U pore velocity

D dispersion tensor (non diagonal)

ω porosity

T_M total mobile concentration

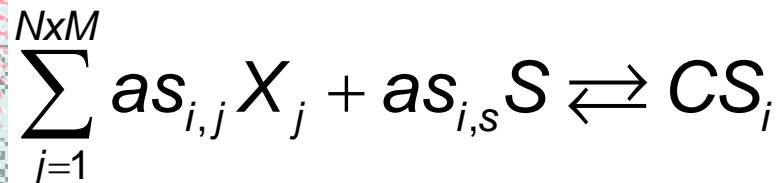
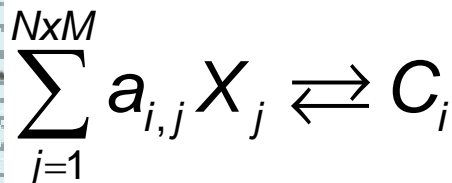
T_F total fixed concentration

Equilibrium chemistry

Mobile Species

Non mobile Species

Reactions



Mass action laws

$$C_i = K_i \cdot \prod_{j=1}^{N \times M} X_j^{a_{i,j}}$$

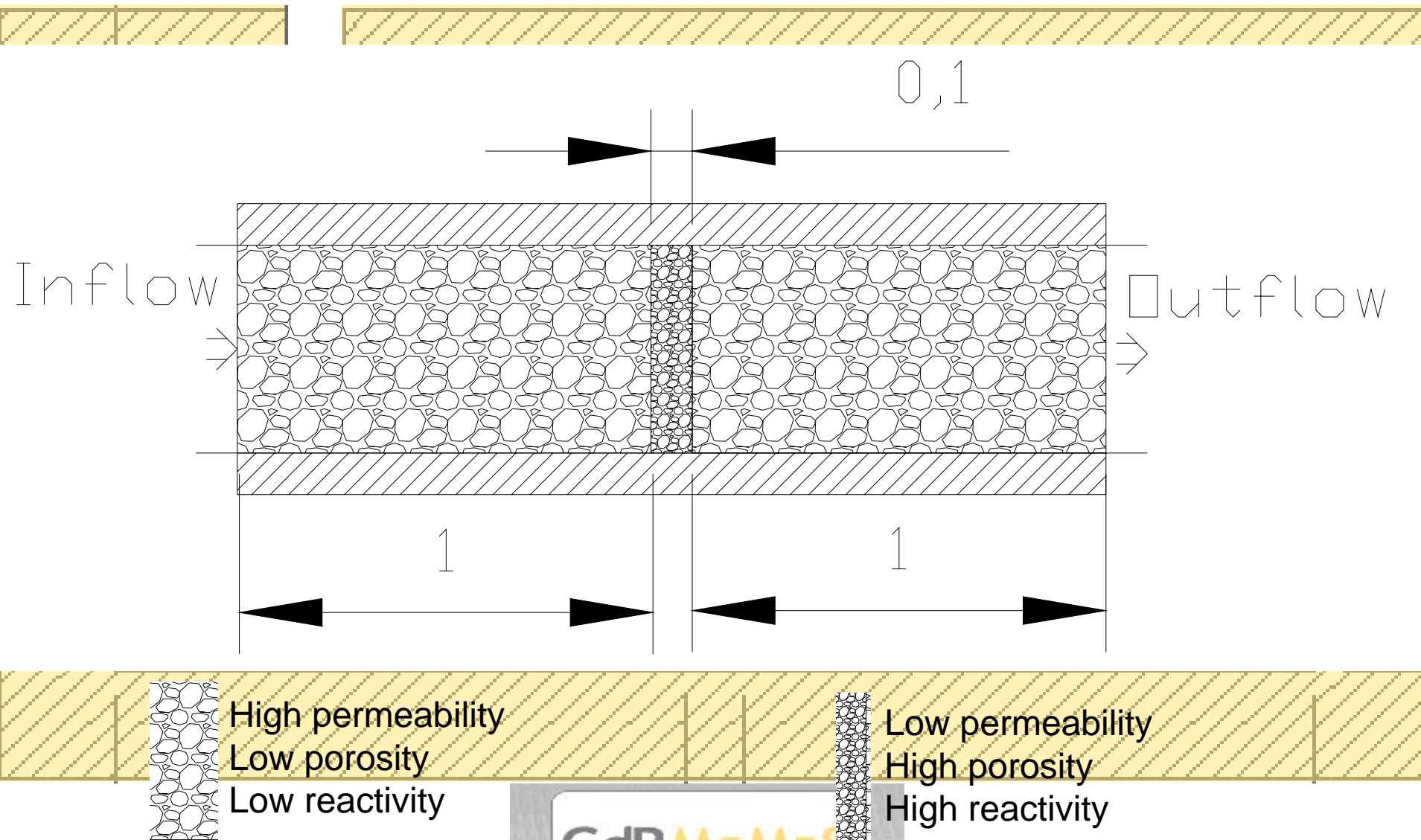
$$CS_i = K_{s_i} \cdot \prod_{j=1}^{N \times M} X_j^{a_{i,j}} \cdot S^{a_{i,s}}$$

Conservation laws

$$T_j = X_j + \sum_{i=1}^{NcM} a_{i,j} \cdot C_i + \sum_{i=1}^{NcS} a_{i,j} \cdot CS_i$$

$$TS = S + \sum_{i=1}^{NcS} a_{i,s} \cdot CS_i$$

The 1D reactive domain



Chemical reactions

	X_1	X_2	X_3	X_4	S	K
C_1	0	-1	0	0	0	1.00E-12
C_2	0	1	1	0	0	1
C_3	0	-1	0	1	0	1
C_4	0	-4	1	3	0	0.1
C_5	0	4	3	1	0	1.00E+35
CS_1	0	3	1	0	1	1.00E+6
CS_2	0	-3	0	1	2	1.00E-01
Total (m.L⁻³)	T_1	T_2	T_3	T_4	TS	
Initial for medium A	0	-2	0	2	1	
Initial for medium B	0	-2	0	2	10	

injected

injected

GdR MoMaS

Some solutions

Refining until convergence...

SPECY

- **SNIA OS scheme**

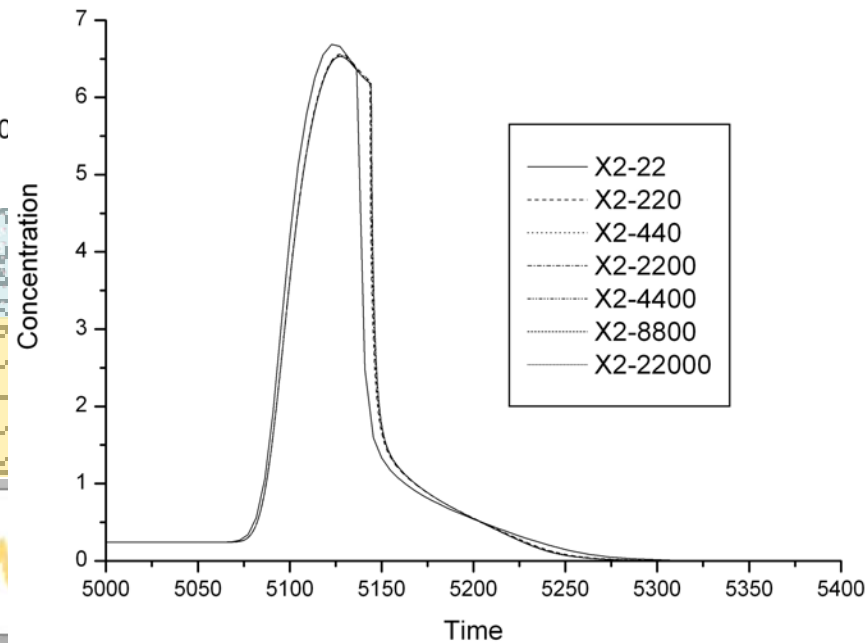
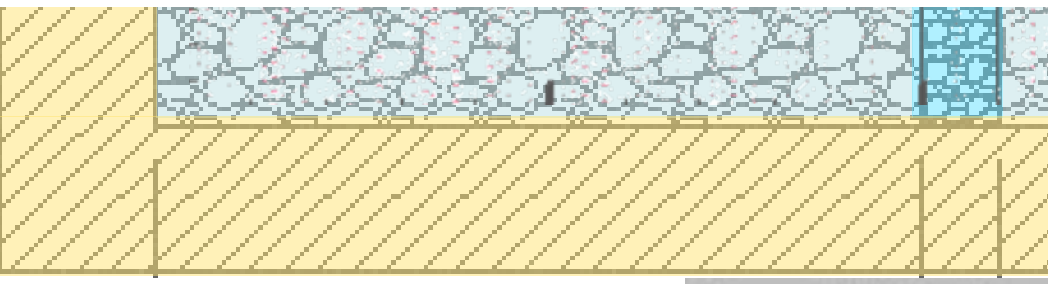
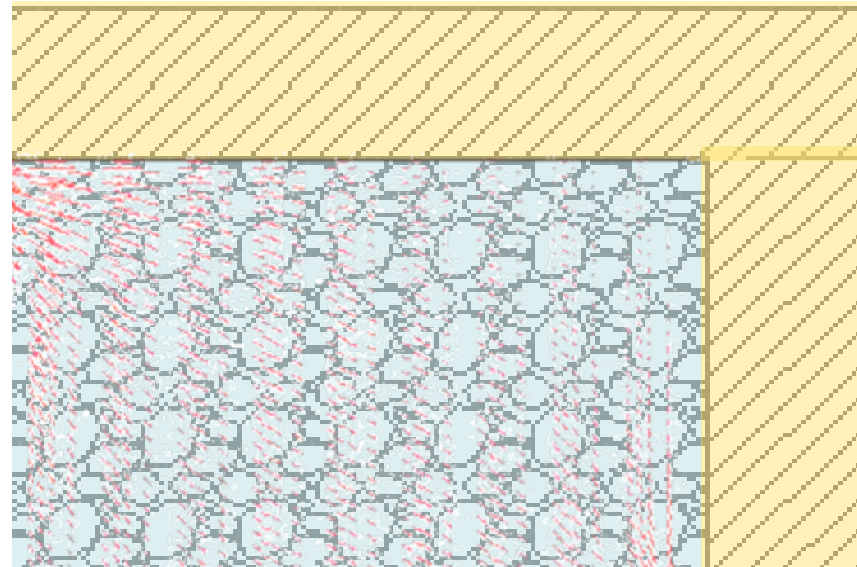
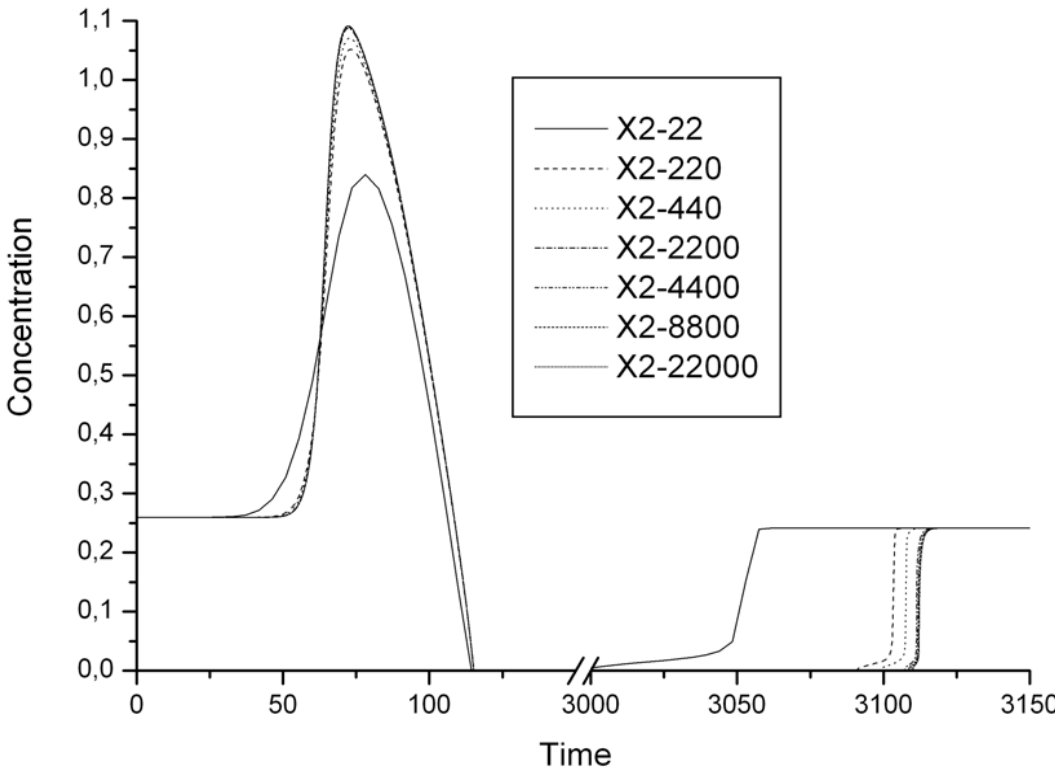
- **Discontinuous finite element for convection**

- explicit time step, constant
- CFL = 1

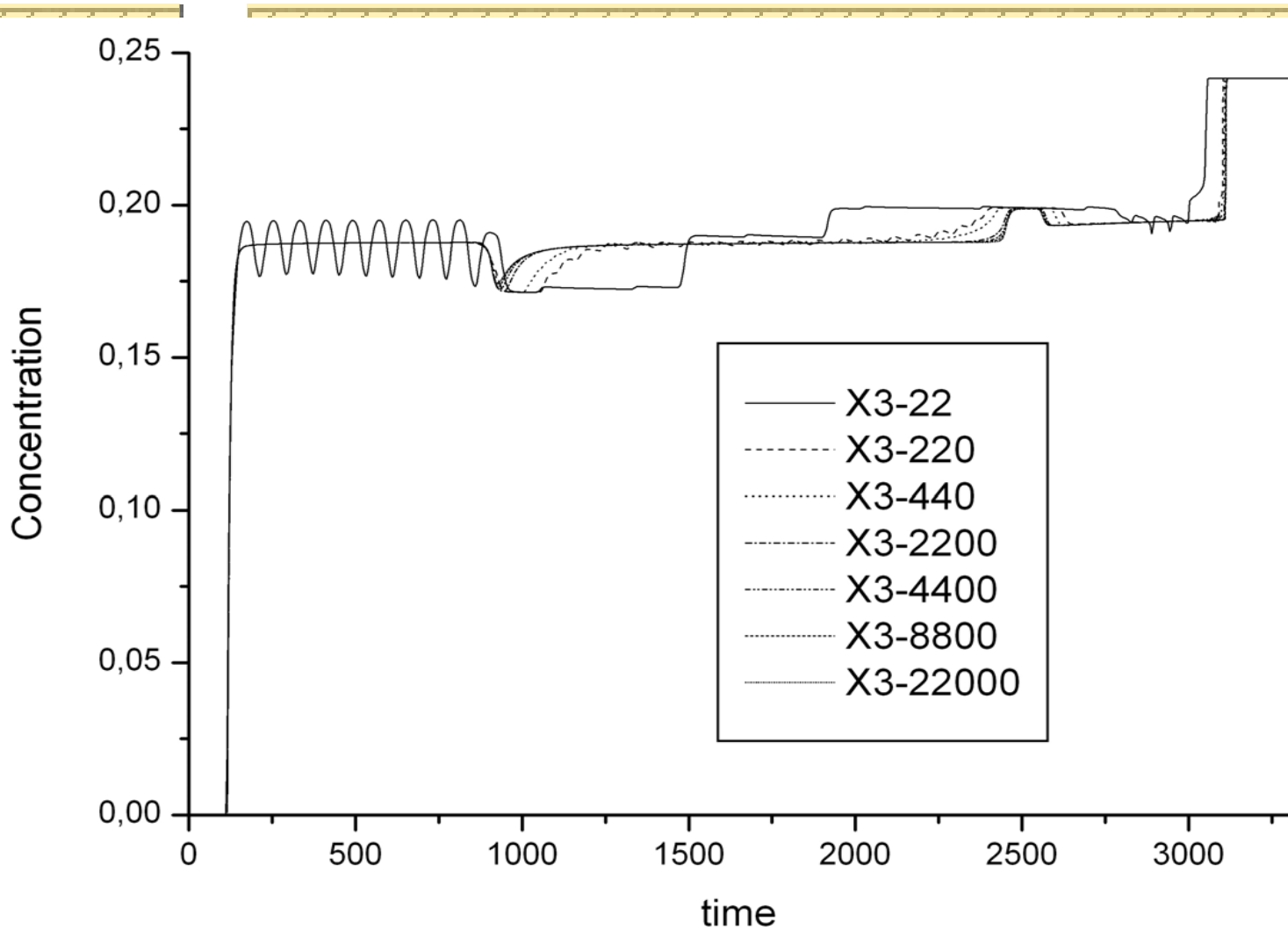
- **Mixed hybrid finite elements for dispersion**

- implicit time step, constant

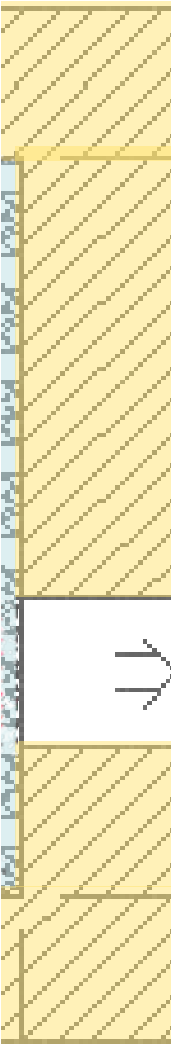
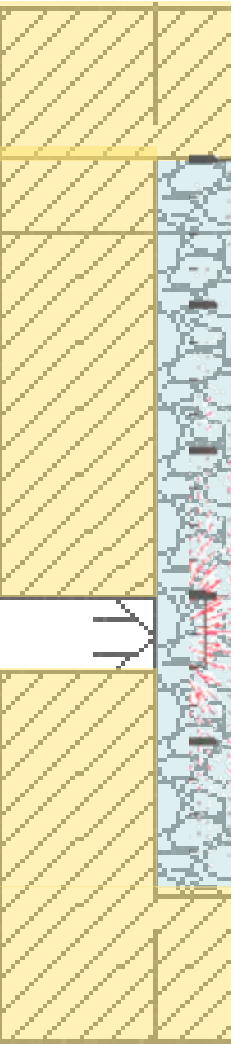
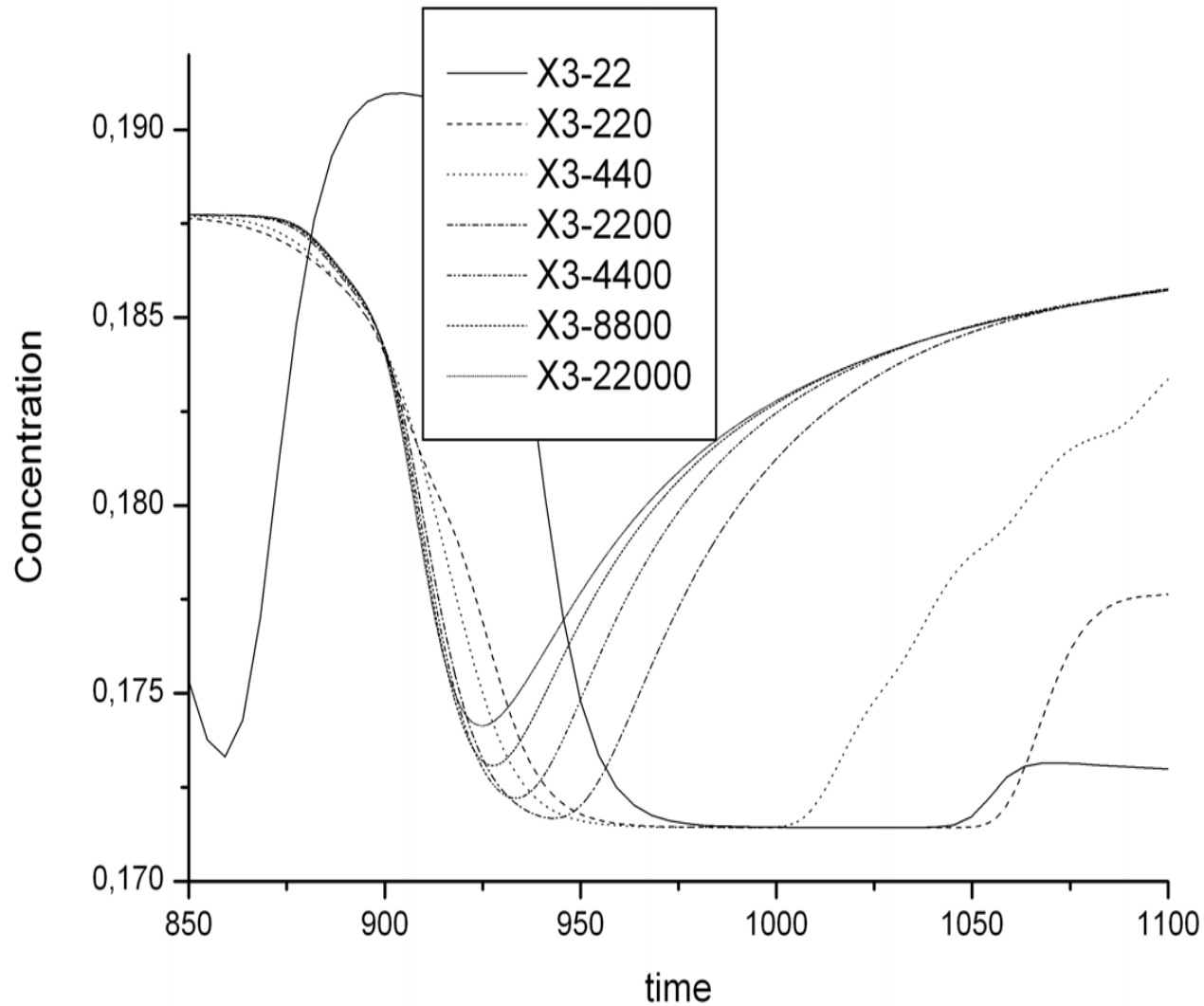
Elution curves for X2



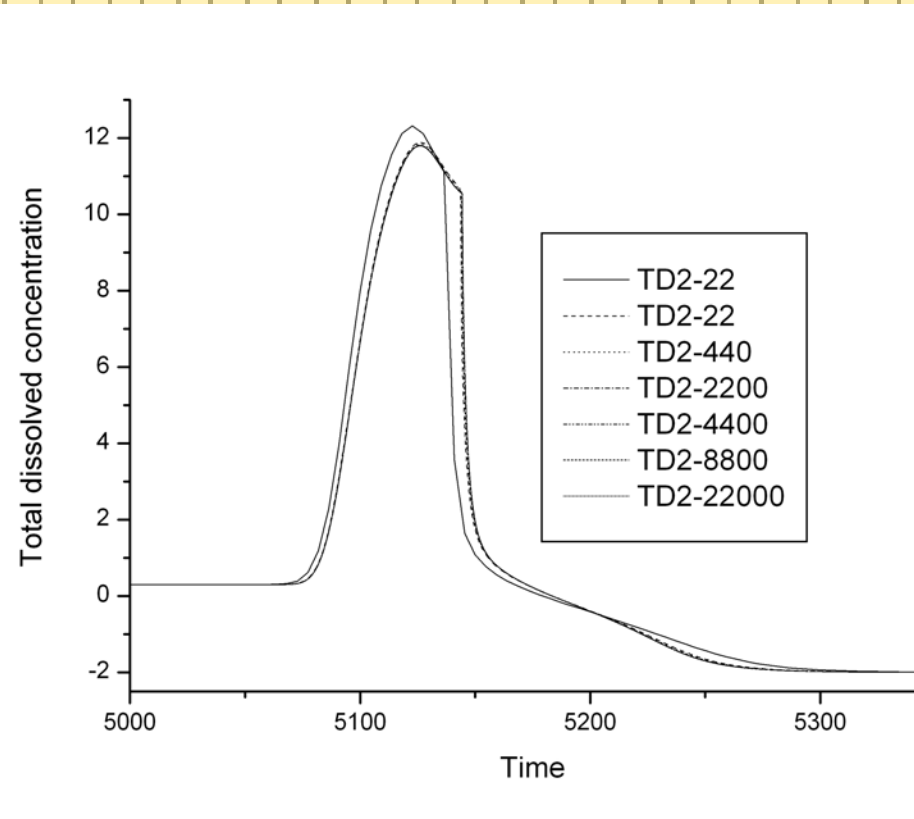
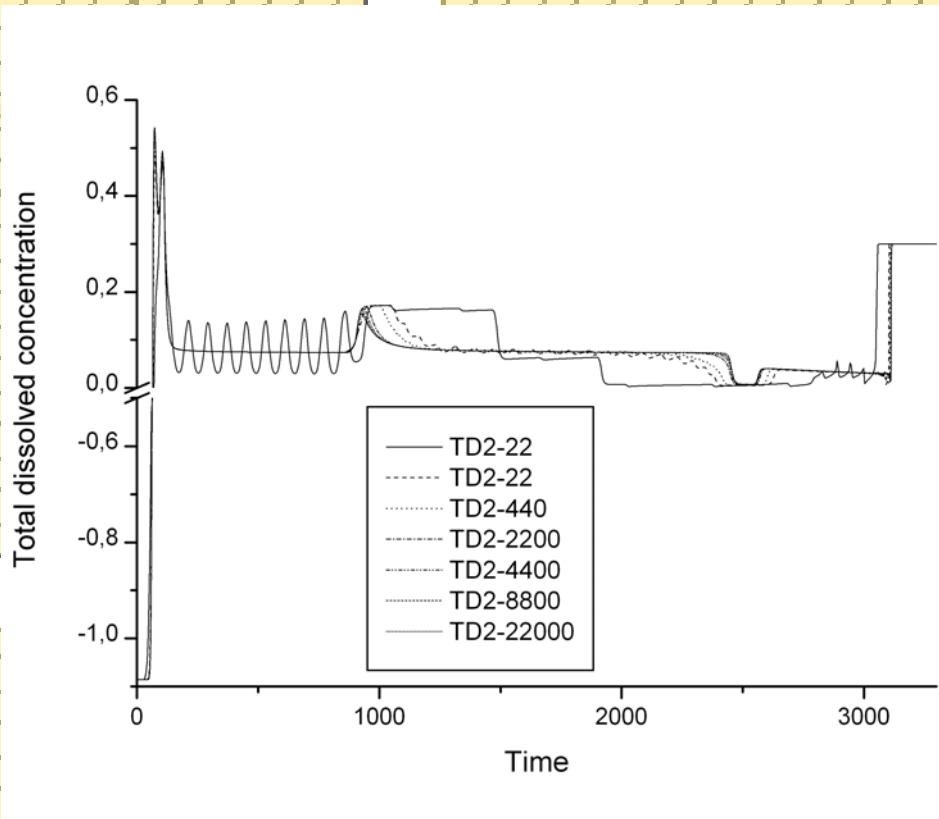
Elution curves for X3



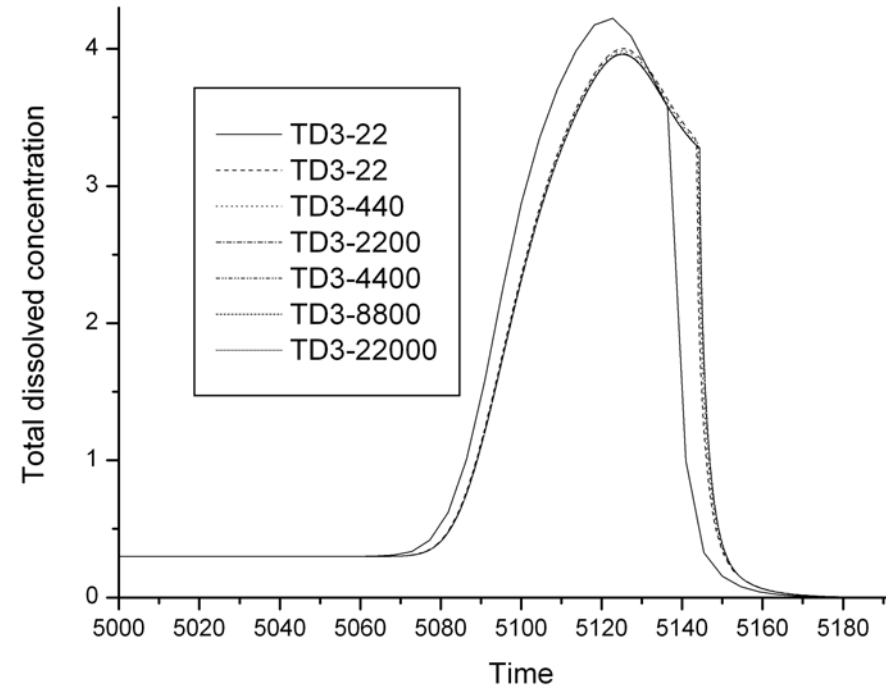
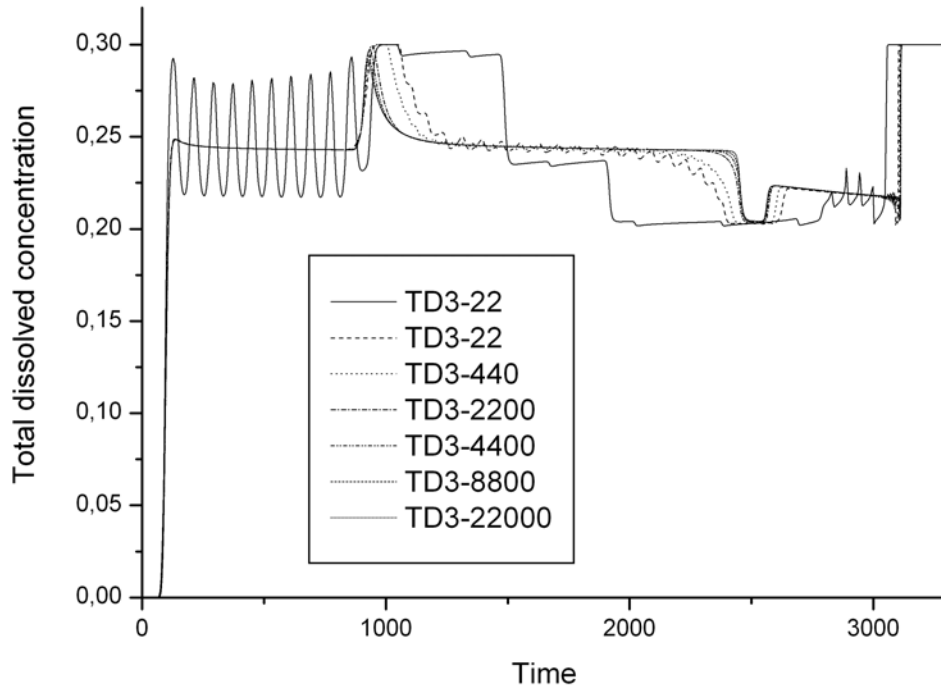
Zoom on elution curves for X3



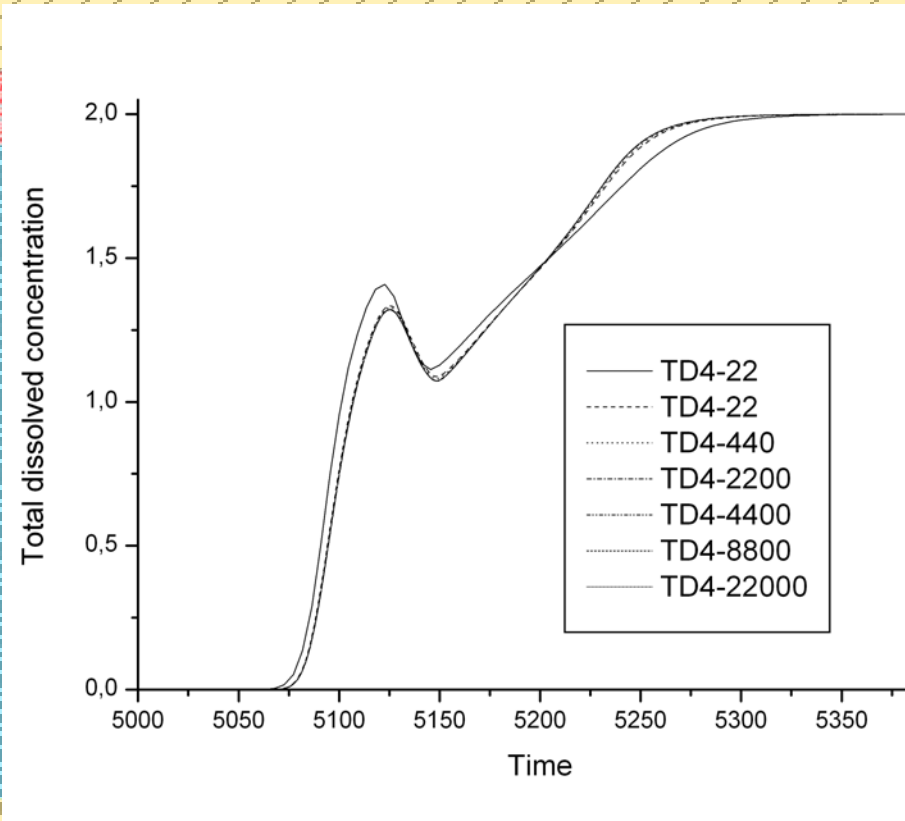
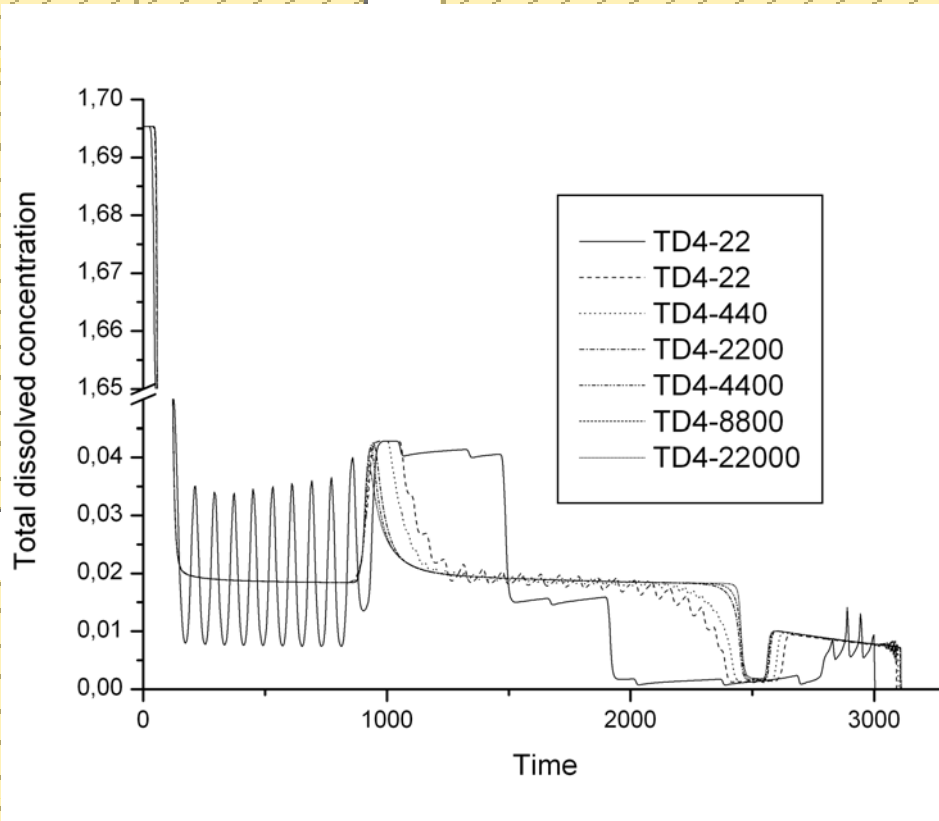
Elution curves for total X2



Elution curves for total X3



Elution curves for total X4



CONCLUSION ?

- Many problems are posed
 - The mesh size is not acceptable for realistic problems
 - Oscillation are generated by interaction between chemistry and transport
 - Some difficulties to solve non linear chemistry are not reported
- This benchmark proposes to test the methods
- International workshop on reactive transport
Strasbourg, January 2008

International workshop on reactive transport Strasbourg January 21-24 2008

- On day is devoted to the presentation of the benchmark results
- 10 000 € Reward for best participations to this benchmark

Conservation of mass

Mobile Species

Non mobile Species

$$T_j = X_j + \sum_{i=1}^{NcM} a_{i,j} \cdot C_i + \sum_{i=1}^{NcS} as_{i,j} \cdot CS_i$$

$$TS = S + \sum_{i=1}^{NcS} as_{i,s} \cdot CS_i$$

$$\Rightarrow T_{M_j} = X_j + \sum_{i=1}^{NcM} a_{i,j} C_i$$

Mobile part

$$T_{M_s} = 0$$

$$T_{F_j} = \sum_{i=1}^{NcS} as_{i,j} \cdot CS_i$$

Fixed part

$$T_{F_s} = S + \sum_{i=1}^{NcS} as_{i,s} \cdot CS_i$$